

# *Modeling and simulation of Microfluidics systems*

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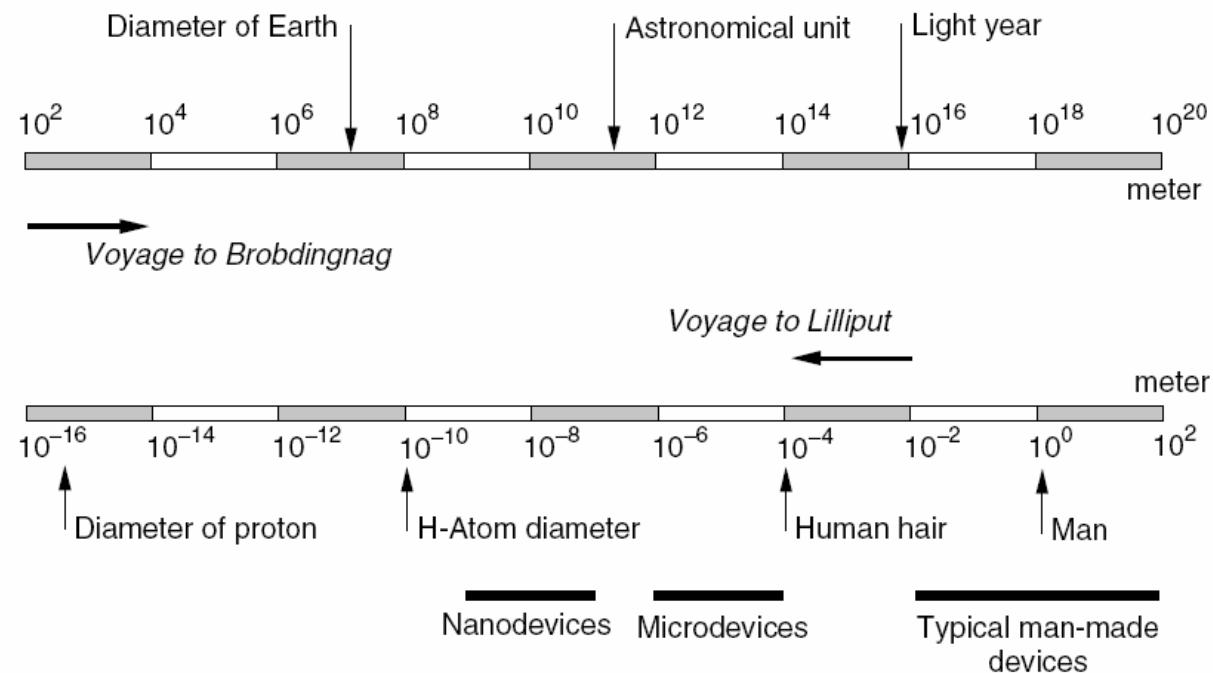


FIGURE 1.1 Scale of things, in meters. Lower scale continues in the upper bar from left to right. One meter is  $10^6$  microns,  $10^9$  nanometers, or  $10^{10}$  Angstroms.

- the nature of phenomena changes with reducing sizes. e.g., gravitational force, surface tension effect, magnetic force, etc.

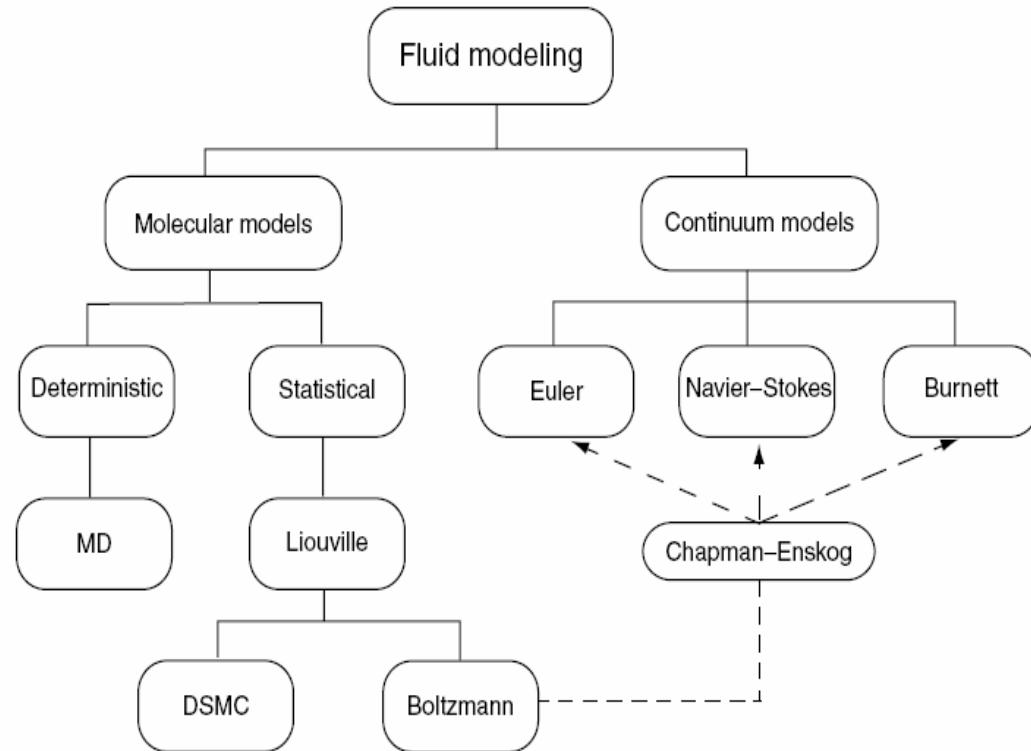


FIGURE 4.1 Molecular and continuum flow models.

$$Kn = \frac{\lambda}{D_h}$$

Knudsen number:  $D_h$  is hydraulics diameter and  $\lambda$  is the mean free path of fluid

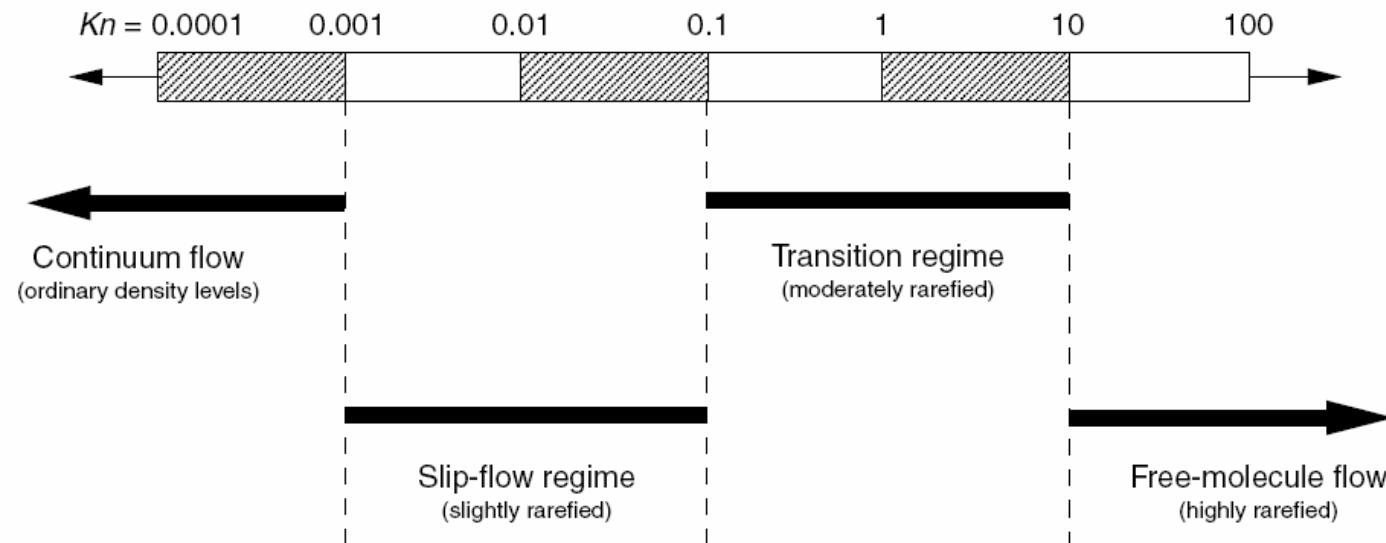
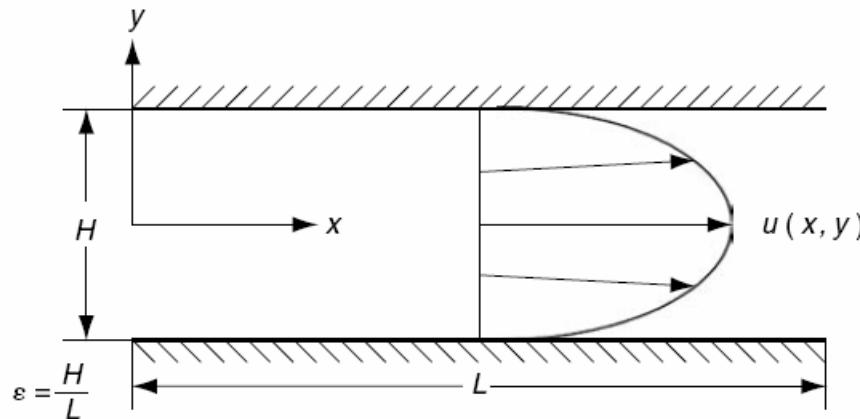


FIGURE 4.2 Knudsen number regimes.

TABLE 8.1 Flow Regimes and Fluid Models

Knudsen Number	Fluid Model
$Kn \rightarrow 0$ (continuum, no molecular diffusion)	Euler equations
$Kn \leq 10^{-3}$ (continuum with molecular diffusion)	Navier–Stokes equations with no-slip-boundary conditions
$10^{-3} \leq Kn \leq 10^{-1}$ (continuum–transition)	Navier–Stokes equations with slip-boundary conditions
$10^{-1} \leq Kn \leq 10$ (transition)	Burnett equations with slip-boundary conditions Moment equations Direct Simulation Monte Carlo (DSMC) Boltzmann equation
$Kn > 10$ (free molecular flow)	Collisionless Boltzmann equation DSMC



In a normal size we can assume that near the wall (at wall-fluid interface), velocity of fluid is zero, but due to the small size in microchannel, this assumption is not true.

To reach this fact, researchers suggest the following expression:

$$U = \left( \frac{2 - \sigma_v}{\sigma_v} \right) Kn \frac{\partial U}{\partial Y} \Big|_{wall} + \frac{3}{2\pi} \frac{(\gamma - 1)}{\gamma} \frac{Kn^2 \text{ Re}}{Ec} \frac{\partial \theta}{\partial X} \Big|_{wall}$$

$$\theta - \theta_{wall} = \left( \frac{2 - \sigma_T}{\sigma_T} \right) \left( \frac{2\gamma}{\gamma + 1} \right) \text{Pr} \left[ Kn \left( \frac{\partial \theta}{\partial Y} \Big|_{wall} \right) + \frac{Kn^2}{2!} \left( \frac{\partial^2 \theta}{\partial Y^2} \Big|_{wall} \right) + \dots \right]$$

$$U = \left( \frac{2 - \sigma_v}{\sigma_v} \right) Kn \frac{\partial U}{\partial Y} \Big|_{wall} + \frac{3}{2\pi} \frac{(\gamma - 1)}{\gamma} \frac{Kn^2 \operatorname{Re}}{Ec} \frac{\partial \theta}{\partial X} \Big|_{wall}$$

$$U - U_{wall} = Kn \frac{\partial U}{\partial Y} \Big|_{wall}$$

$$\theta - \theta_{wall} = \left( \frac{2 - \sigma_T}{\sigma_T} \right) \left( \frac{2\gamma}{\gamma + 1} \right) \frac{1}{\operatorname{Pr}} \left[ Kn \left( \frac{\partial \theta}{\partial Y} \Big|_{wall} \right) + \frac{Kn^2}{2!} \left( \frac{\partial^2 \theta}{\partial Y^2} \Big|_{wall} \right) + \dots \right]$$

$$\theta - \theta_{wall} = \frac{Kn}{\beta} \frac{\partial \theta}{\partial Y} \Big|_{wall}$$

## Boundary condition:

Inlet ( $x=0$ ):  $u=u_{in}$ ,  $v=0$  and  $T=T_{in}$

Outlet ( $x=L$ ):  $\frac{\partial \Phi}{\partial x} = 0$

where  $\Phi = u, v, T$

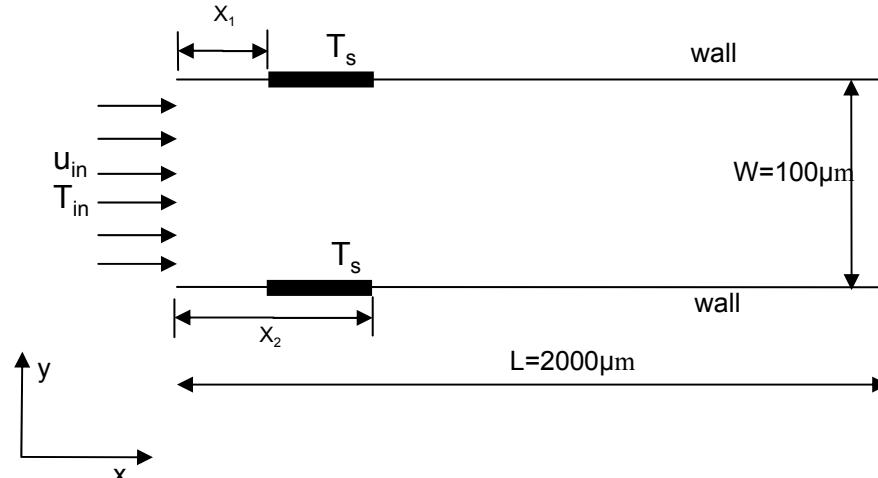
but  $p=0$

At wall ( $y=0, y=W$ ):

$u=v=0, x_1 \leq x \leq x_2: T = T_s$

$0 \leq x < x_1 \text{ and } x_2 < x \leq L: T = T_0$

also: near the wall  $\dot{U} - U_{wall} = Kn \frac{\partial U}{\partial Y} \Big|_{wall}$



$$\theta - \theta_{wall} = \frac{Kn}{\beta} \frac{\partial \theta}{\partial Y} \Big|_{wall} \quad \beta = \left( \frac{\gamma + 1}{\gamma} \right) Pr$$

## Implementation of Boundary slip conditions

$$U_N - U_{wall} = Kn \frac{\partial U}{\partial Y} \Big|_{wall}$$

$$\frac{\partial U}{\partial Y} = \frac{U_P - U_N}{\Delta Y}$$

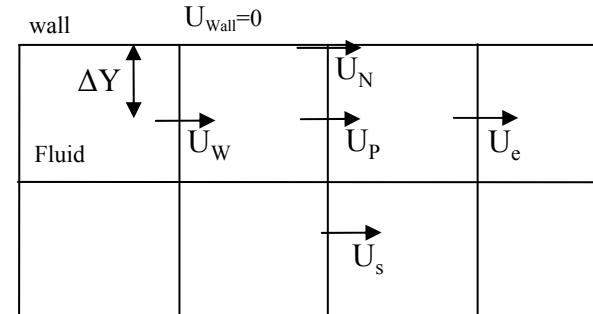
$$U_P - U_N = \frac{(U_P - U_{wall})}{\left(1 + \frac{Kn}{\Delta Y}\right)}$$

$$a_N (U_N - U_p) + a_s (U_s - U_p) + a_E (U_E - U_p) + a_w (U_w - U_p) + b = 0$$

$$a_N^* (U_{wall} - U_p) + a_s (U_s - U_p) + a_E (U_E - U_p) + a_w (U_w - U_p) + b = 0$$

$$a_N^* = \frac{a_N}{\left(1 + \frac{Kn}{\Delta Y}\right)}$$

$$a_N^* = \frac{a_N}{\left(1 + \frac{1}{\beta} \frac{Kn}{\Delta Y}\right)}$$



## Navier-Stokes Equations

Continuity: 
$$\frac{\partial u_j}{\partial x_j} = 0$$

Momentum: 
$$\frac{\partial}{\partial x_j} (\rho u_i u_j) = \frac{\partial}{\partial x_j} \left( \mu \left( \frac{\partial u_i}{\partial x_j} \right) \right) - \frac{\partial p}{\partial x_i}$$

Energy: 
$$\frac{\partial}{\partial x_i} (\rho c_p u_i T) = k \frac{\partial}{\partial x_i} \left( \frac{\partial T}{\partial x_i} \right)$$

## Non-dimensional equations

$$X_i = \frac{x_i}{D_h} \quad , \quad U_i = \frac{u_i}{u_{in}} \quad , \quad \theta = \frac{T - T_{in}}{T_{wall} - T_{in}} \quad , \quad P = \frac{p}{\rho u_{in}^2}$$

$$D_h = \frac{4A}{S} \quad , \quad D_h = \frac{4WH}{2(W+H)} \quad \text{and also } H \gg W \text{ So: } D_h = 2W$$

$$\text{Pr} = \frac{\mu c_p}{k} \quad , \quad \text{Re} = \frac{\rho u_{in} D_h}{\mu} \quad , \quad Pe = \text{Re} \text{Pr}$$

**Continuity:**  $\frac{\partial U_j}{\partial X_j} = 0$

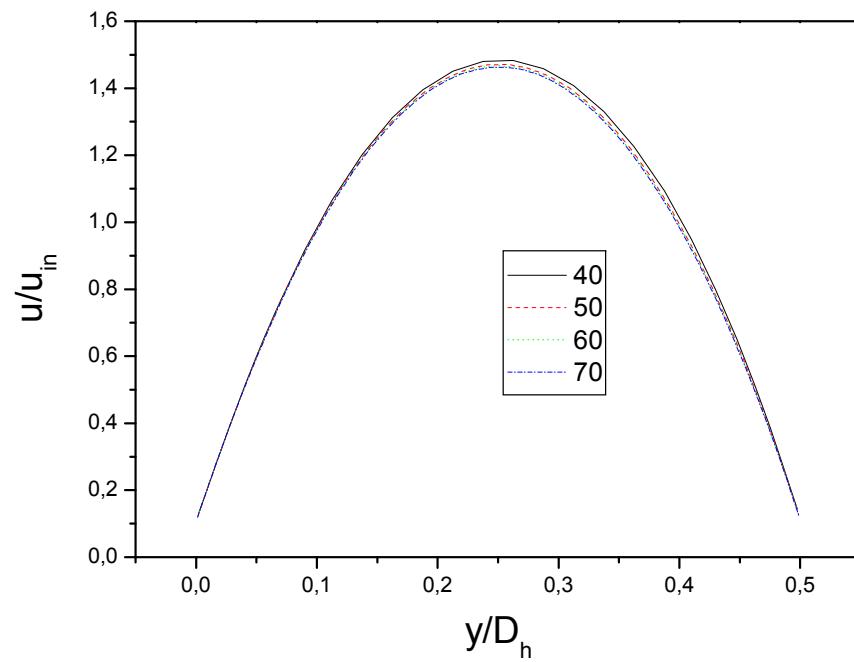
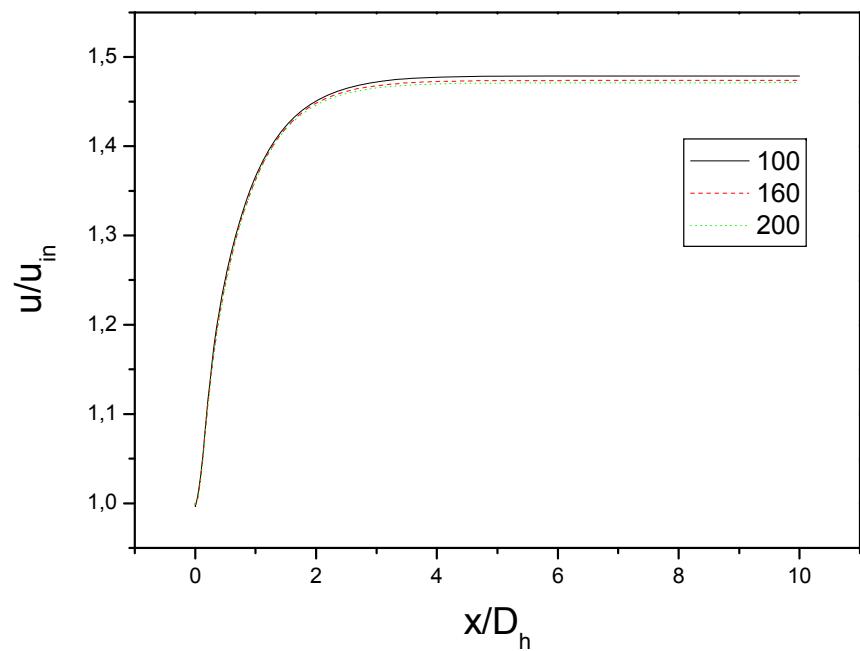
**Momentum:**  $\frac{\partial}{\partial X_j} (U_i U_j) = \frac{1}{\text{Re}} \left( \frac{\partial^2 U_i}{\partial X_j^2} \right) - \frac{\partial P}{\partial X_i}$

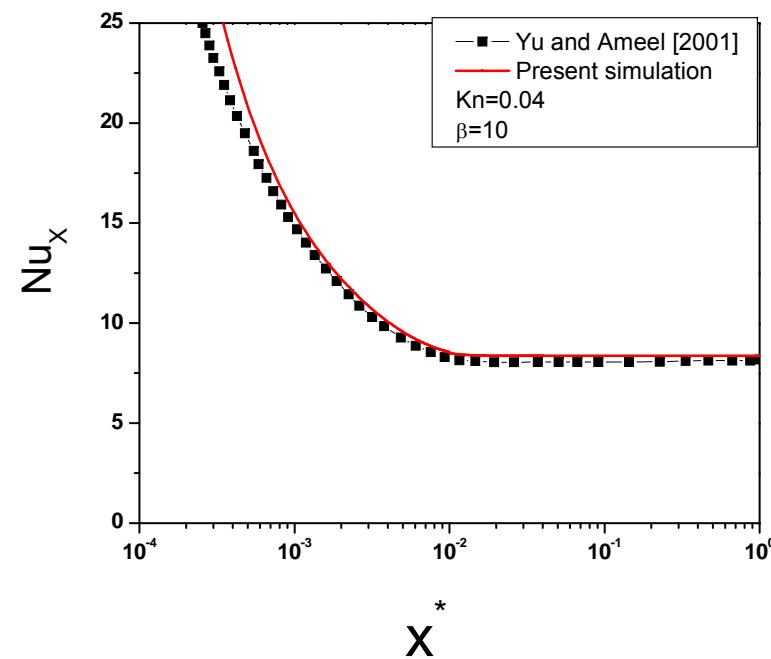
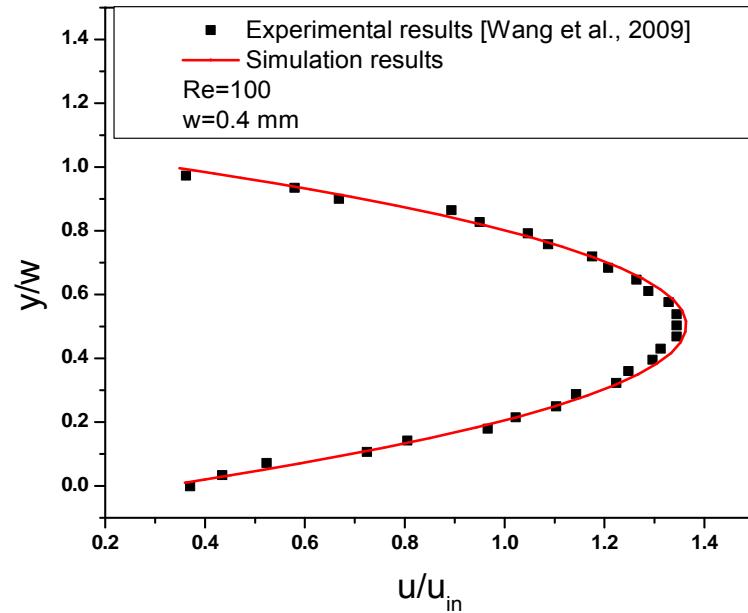
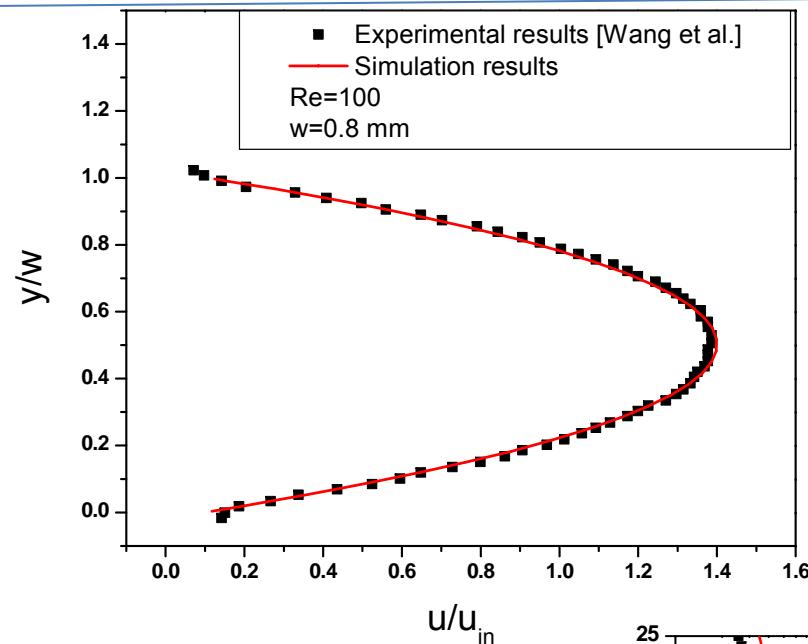
**Energy:**  $\frac{\partial}{\partial X_i} (U_i \theta) = \frac{1}{Pe} \frac{\partial^2 \theta}{\partial X_i^2}$

## Numerical procedure

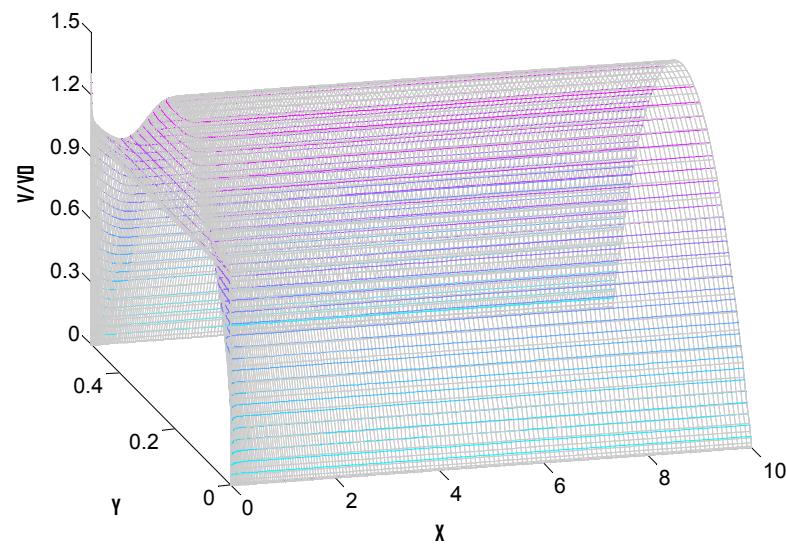
- *Control volume technique*
- *Power law scheme*
- *SIMPLER( Semi-Implicit Method for Pressure-Linked Revised Equations)*
- The discretization grid is non-uniform. It is finer near the tube entrance and near the wall where the velocity and temperature gradient are significant.

## Validation and Comparison

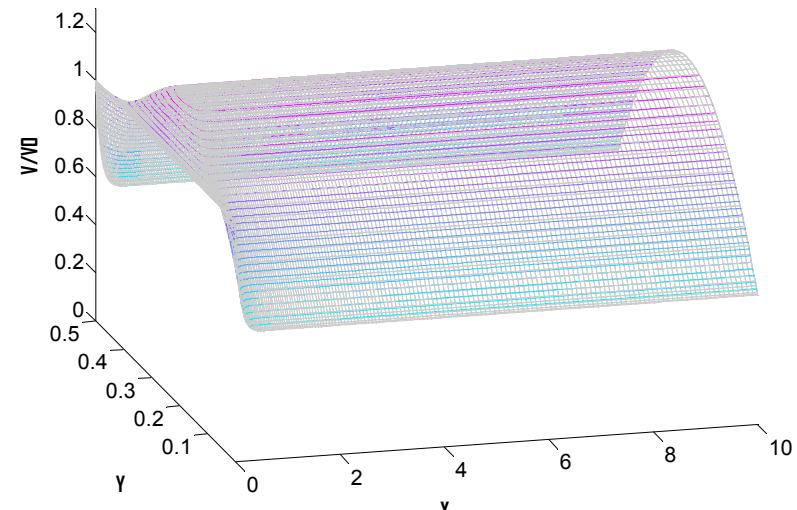




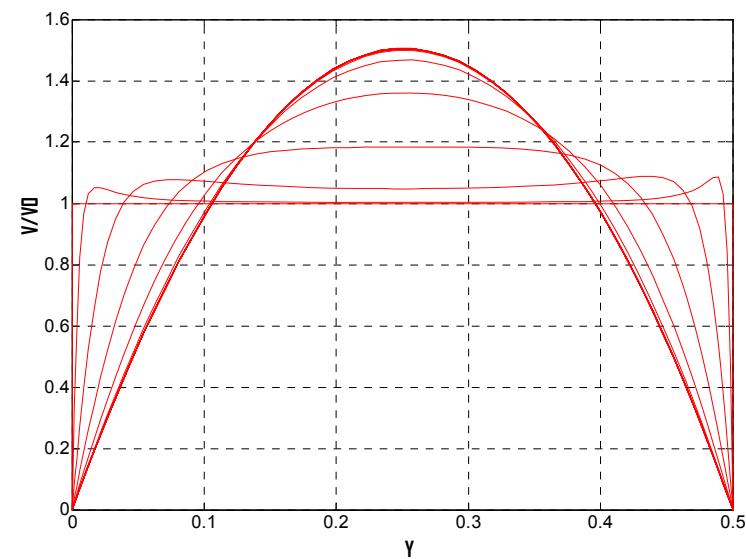
## Contour of the velocity in x direction



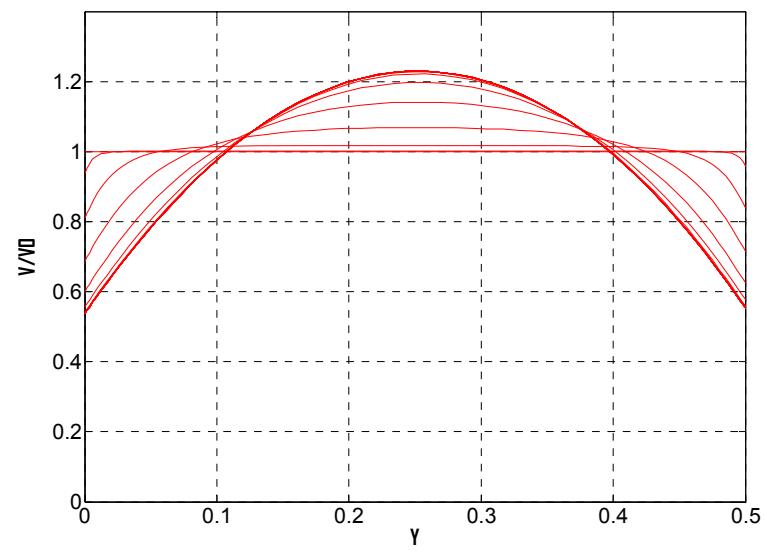
$\text{Kn}=0$



$\text{Kn}=0.1$



$Kn=0$



$Kn=0.1$

Thanks for your consideration